



Thermal storage and model predictive control for improved utilization of industrial waste heat in district heating

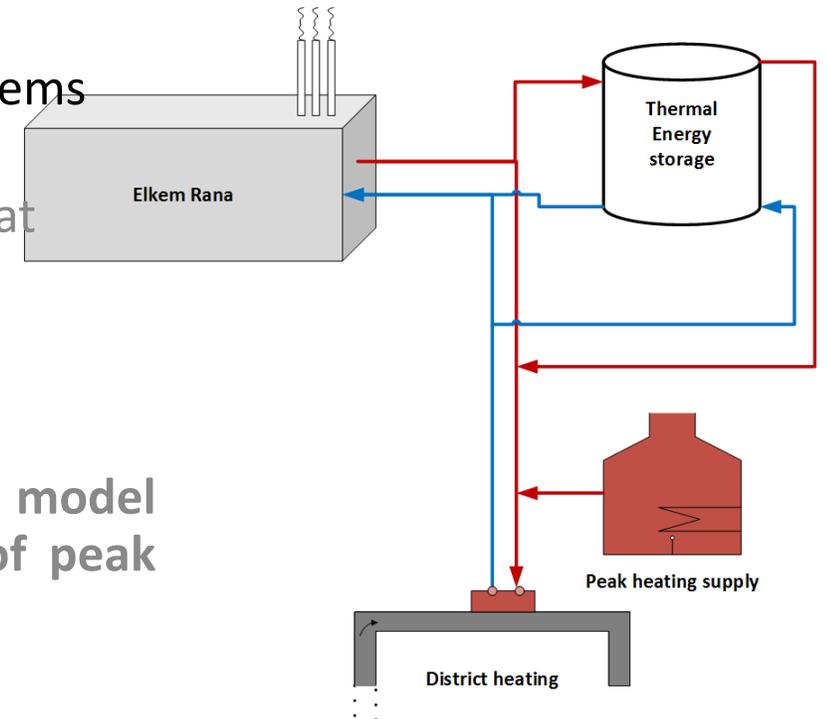
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SINTEF Energy Research / Mo Fjernvarme

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Motivation

- Industrial surplus heat has high potential for utilization in DH
 - Total amount of heat available often larger than the demand, but peak heating required due to temporal mismatch in availability / demand
- Thermal energy storage (TES) widely applied in DH systems utilizing heat sources with predictable output
 - More challenging in a system utilizing a surplus heat source with fluctuating output
- Goal for the study
 - Analyze the potential of TES in combination with model predictive control (MPC) to minimize the use of peak heating at Mo Fjernvarme





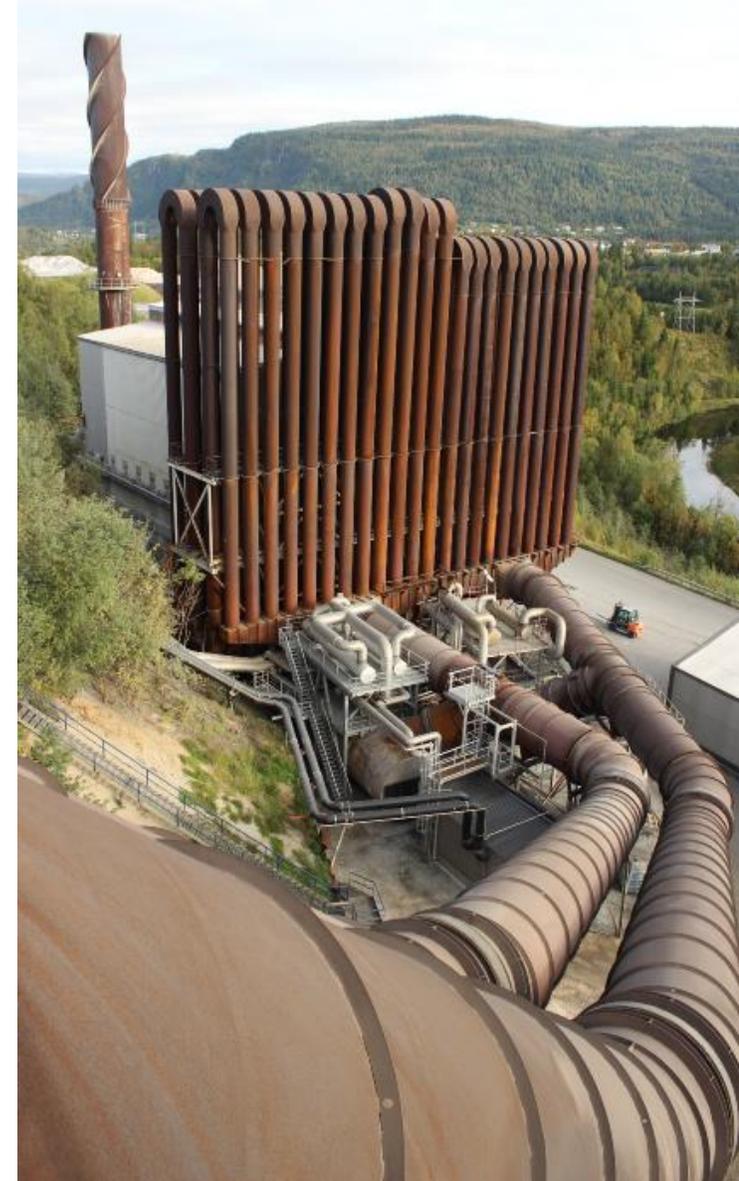
Case study description

District heating in Mo i Rana

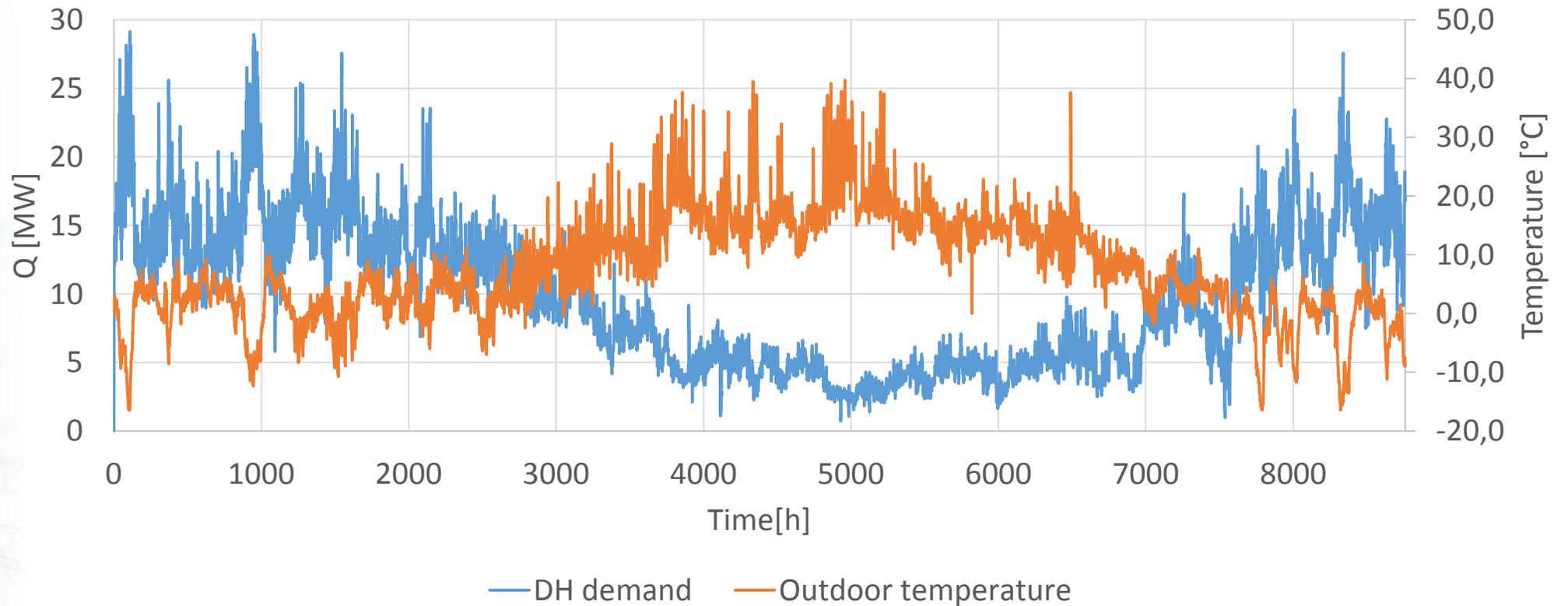
DH production in Mo i Rana



- Mo Fjernvarme: Utilizing surplus heat from Mo Industry Park for DH
 - Heat source: off-gases from FeSi production plant
- Amount of waste heat available exceeds the demand
 - Large fluctuations in availability
 - Peak boilers: CO-gas, electricity, oil



The climate and total DH demand in 2017



Total DH demand: **84 GWh**

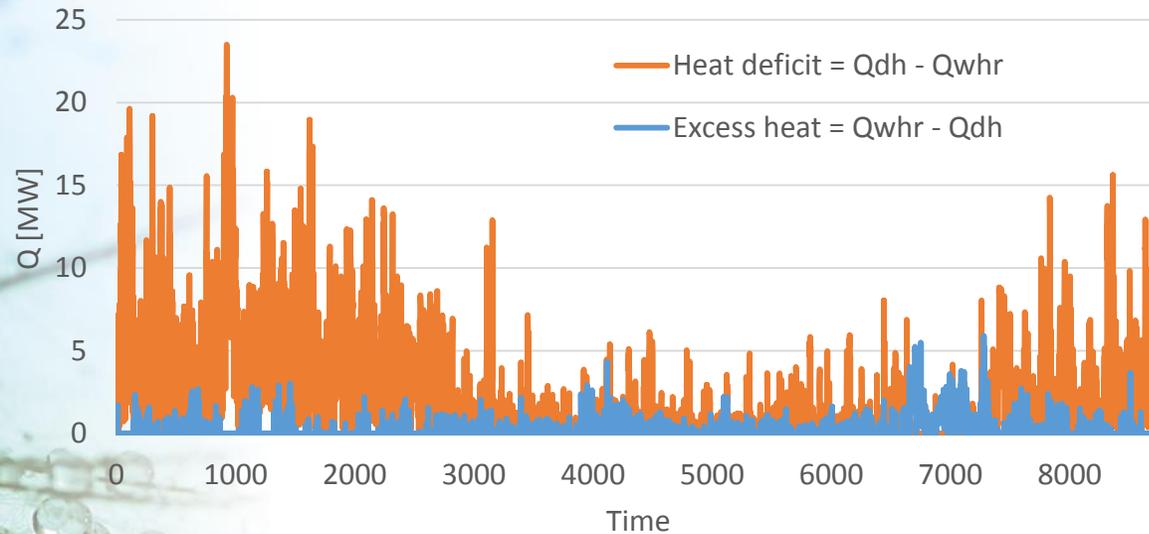
Total peak heating demand: **18 GWh**

→ **21 %** of the total production / **94 %** of the heat production costs

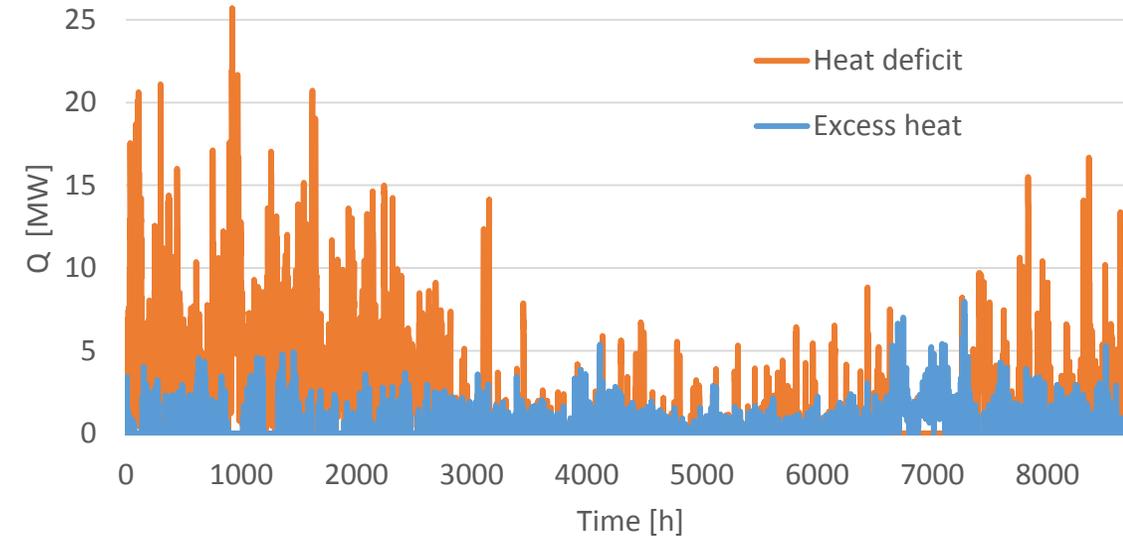
→ 2017 was not a representative year!

Potential for TES?

Present situation



Future scenario



Could TES be used to recover some of the rejected heat, to reduce use of peak heating?

- Future scenario
 - 20 % increase in surplus heat production
 - 10 % increase in the demand

	Current	Future
Total excess heat [GWh]	1.4	3.4
Total heat deficit [GWh]	19.1	16.1



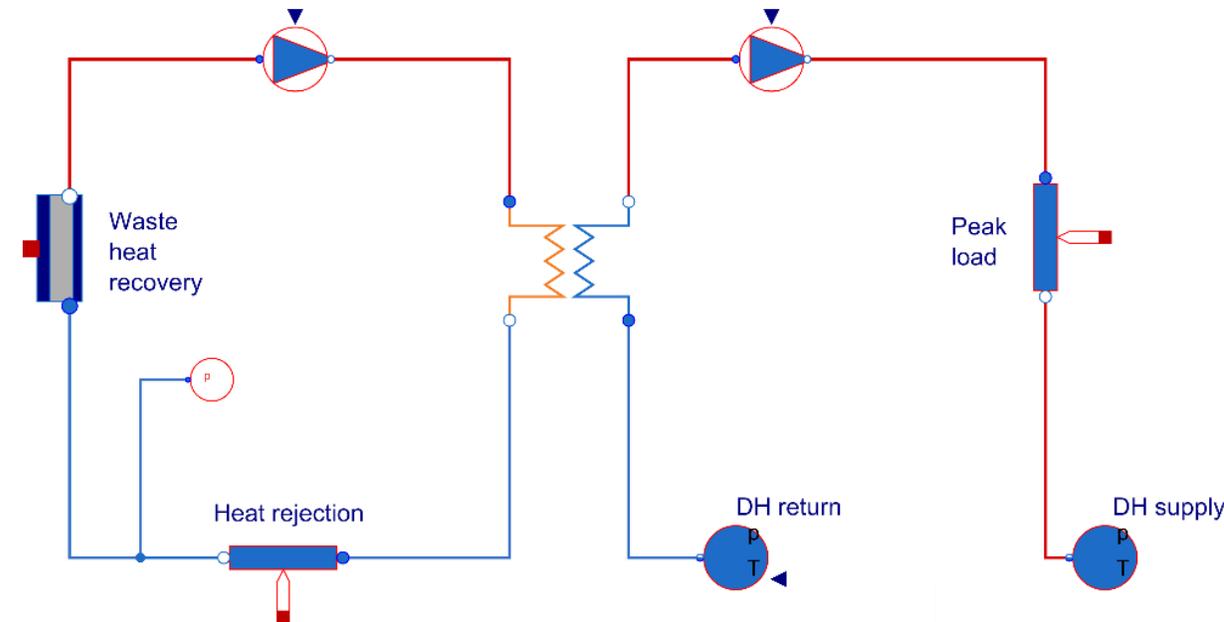
Methodology

Modelling approach

- Dynamic modelling using Dymola / Modelica
 - MPC implemented with jModelica
 - iPopt med Casadi applied to solve dynamic optimal control problems
- Measurement data for heat demand and production for 2017
- **3 scenarios** evaluated for **December 2017**:
 1. Baseline – future scenario with no TES
 2. With TES, "normal" control strategy
 3. With TES + MPC

Scenario 1: Baseline scenario

- **Objective:** Dimension component models and validate the model towards measurement data
- **Simplifications**
 - Water as the working fluid everywhere
 - The DH grid modeled as an open loop with supply & return temperatures and mass flow based on data

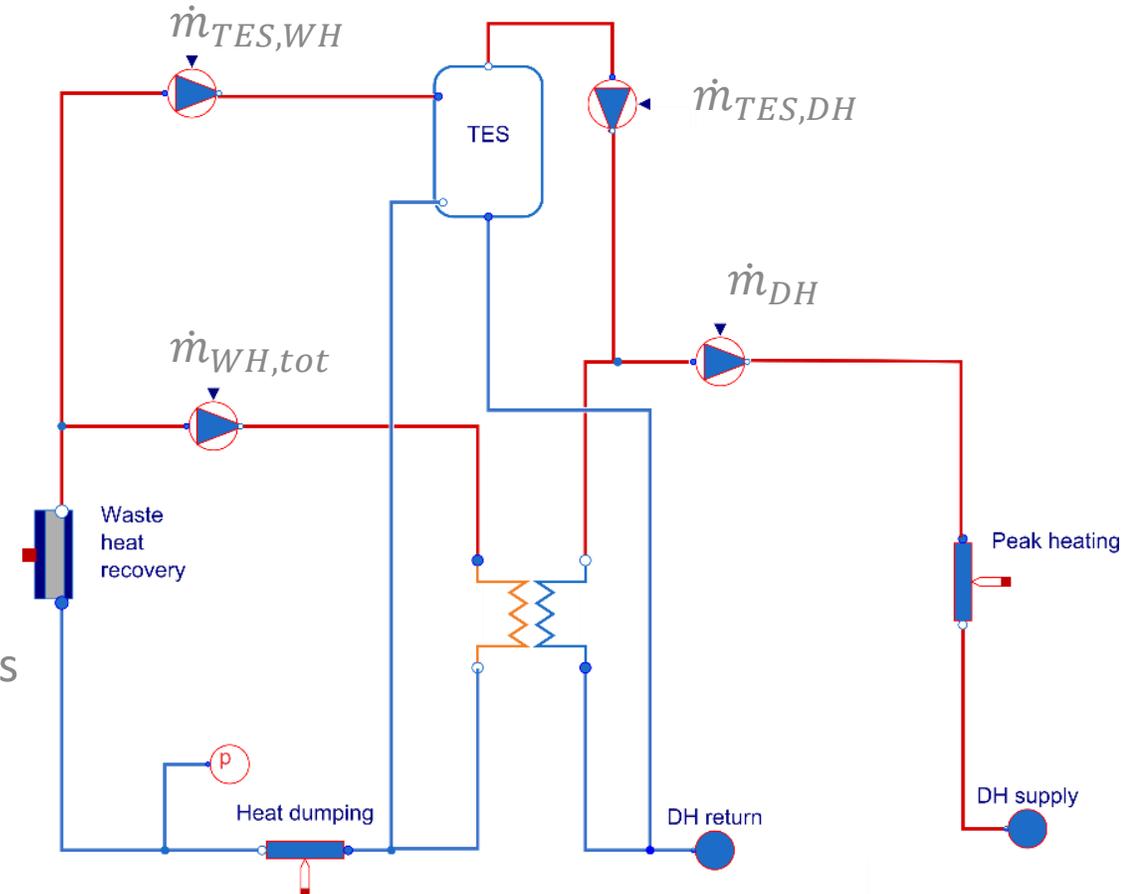


Scenario 2: TES and regular control strategy

- Control strategy:
 - Charge when excess heat available:

$$\dot{m}_{TES,WH} = \max\left(0, \frac{\dot{Q}_{WH} - \dot{Q}_{DH}}{\dot{Q}_{WH}} \dot{m}_{WH,tot}\right)$$
 - Discharge when there is a heat deficit:

$$\dot{m}_{TES,DH} = \max\left(0, \frac{\dot{Q}_{DH} - \dot{Q}_{WH}}{\dot{Q}_{DH}} \dot{m}_{DH}\right)$$
 - Temperature at the top of the tank needs to be at the level of the supply temperature
 - Try to keep the tank temperature at the bottom below 105 °C (max. supply temperature level)



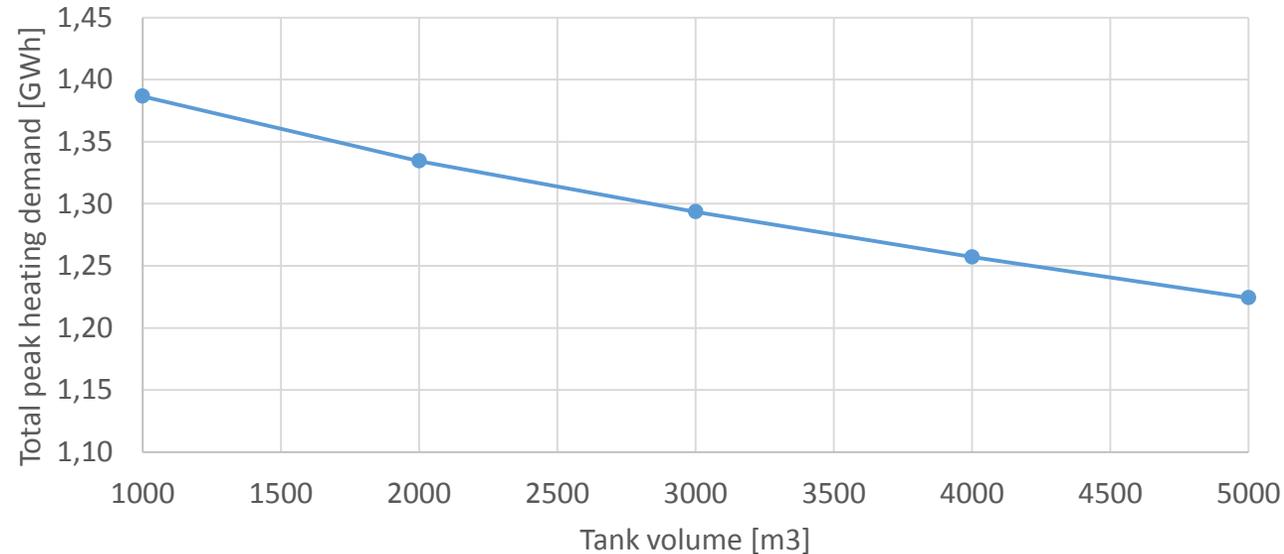
Scenario 2: TES and regular control

Dimensioning of the tank

Selected tank size: 3000 m³

- 7 % reduction in total peak heating demand for December
- Total heat capacity: 175 MWh, corresponding to ca. 50 % of the average daily DH demand in December
- Storage discharge capacity: 8 MW at a mass flow rate of 40 kg/s
 - Approximately 50 % of max. peak heating supply

Tank volume [m ³]	Reduction in peak heating demand (%)
1000	0.5 %
2000	4.3 %
3000	7.2 %
4000	9.8 %
5000	12.2 %

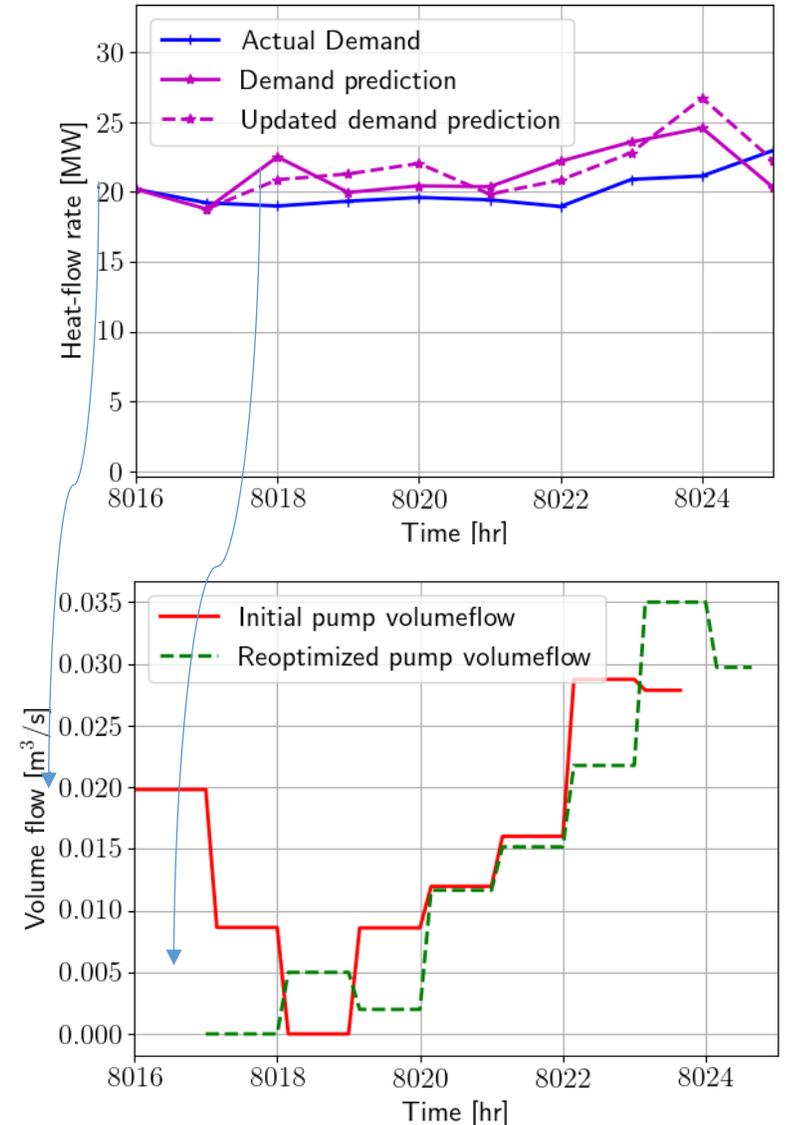


Scenario 3: TES and model predictive control

- Multivariable control of pumps, peak heating and heat rejection.
- Exploit predicted heat demand to optimally control TES in/outflow and minimize peak heating.
- Natural way of handling constraints (satisfaction of demand, pumpflows, max. TES temperature)
- Feedback introduced by re-optimizing control inputs on a receding horizon.

Setup:

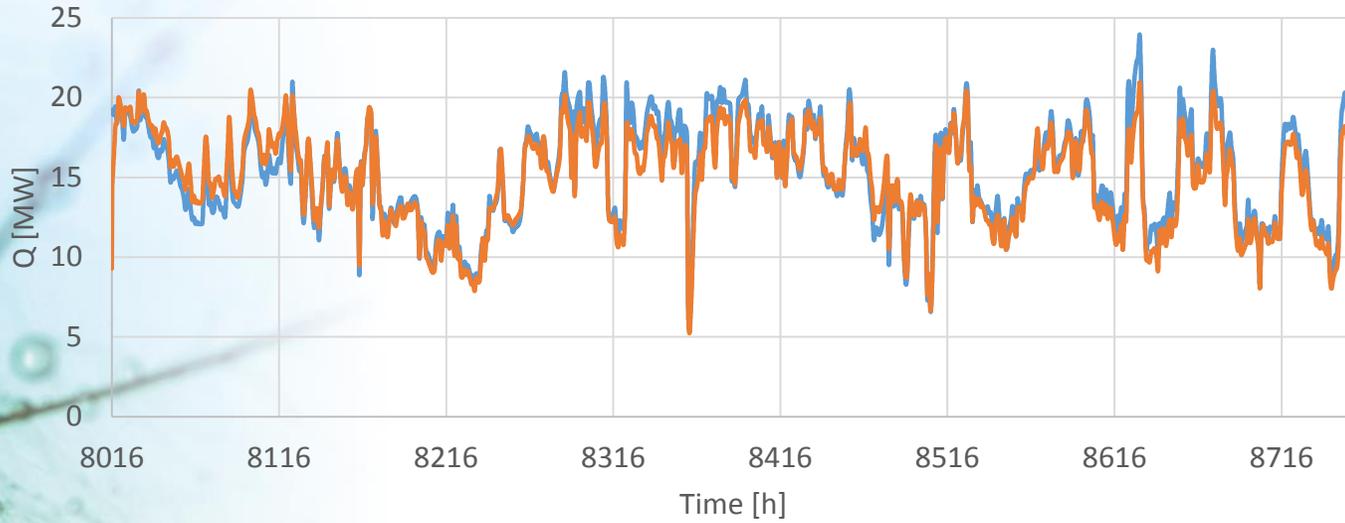
- 12h prediction horizon; reoptimize pump flow velocities and peak heating each hour.
- Demand prediction not implemented - use demand data with added noise to emulate uncertainty in predictions.



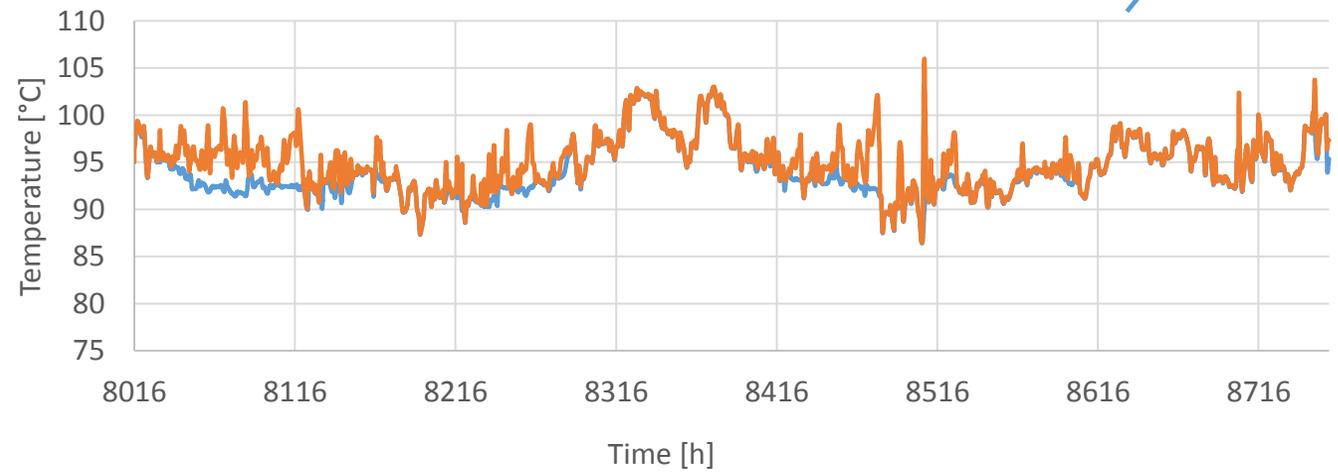
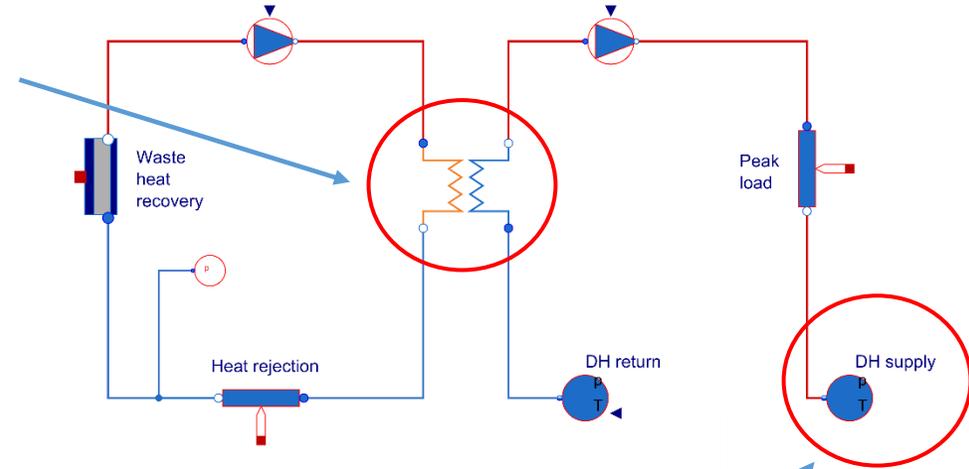


Results

Scenario 1: Baseline

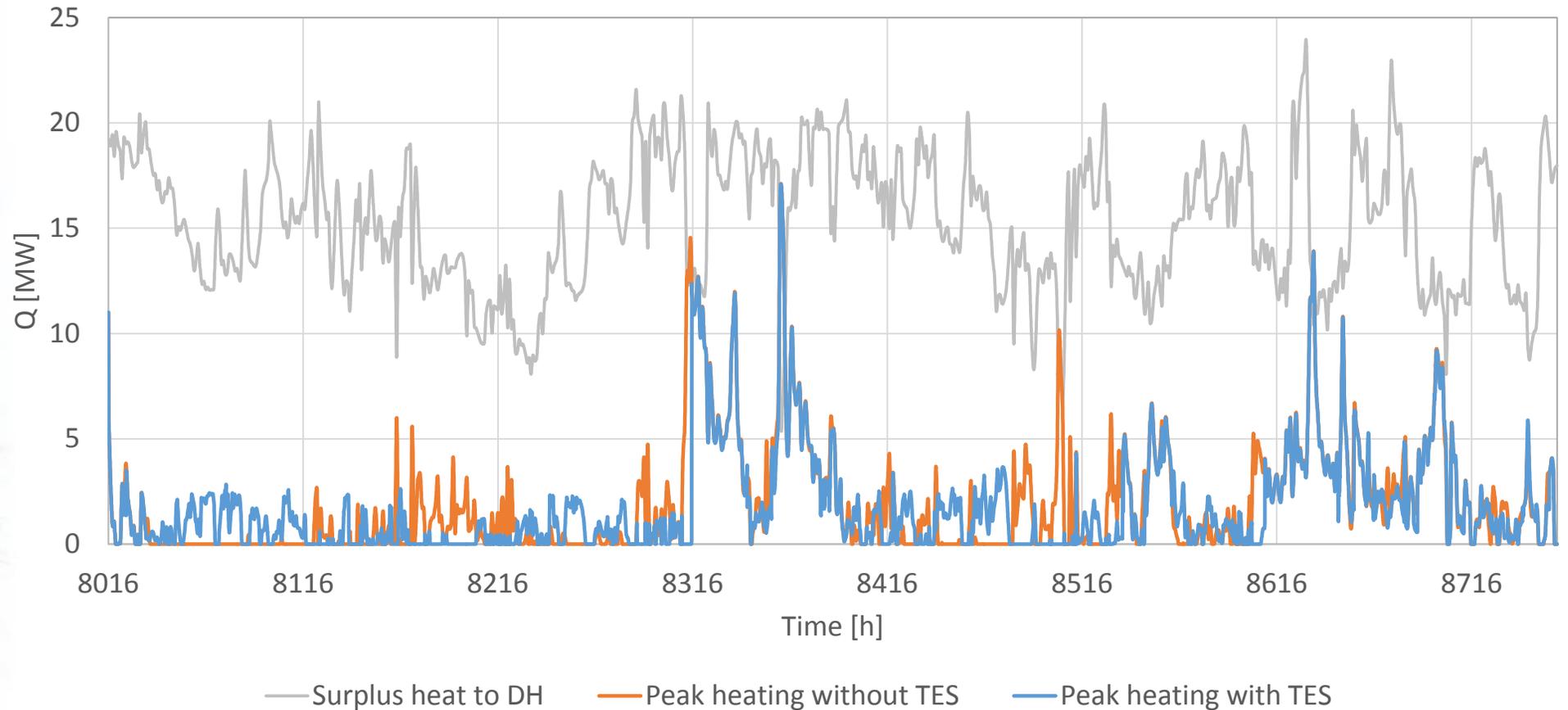


— $Q_{wh,data}$ [MW] — $Q_{wh,model}$ [MW]

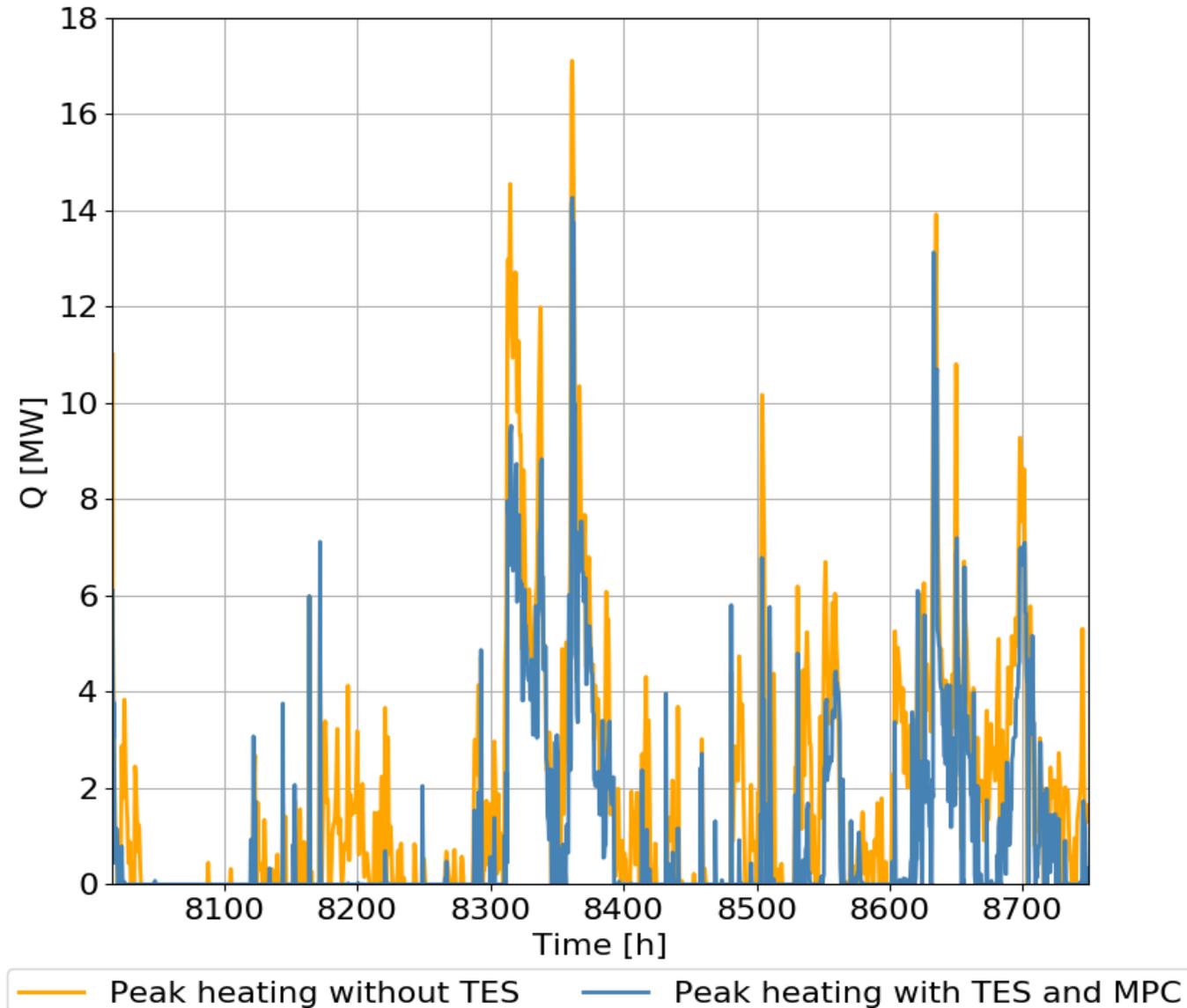


— $T_{supply,data}$ [C] — $T_{supply,model}$ [C]

Scenario 2: TES and regular control – results



Scenario 3: TES and MPC



Comparison

	Basecase	With TES	Reduction from basecase (%)	With TES+MPC	Reduction from basecase (%)
Total peak heating [MWh]	1394	1294	7.20 %	707	49.3%
Max peak heating [MW]	17.1	17.1	0.03 %	14.2	17.0%
Total heat dumping [MWh]	1121	1043	6.93 %	549	51.1%

Concluding remarks

- Industrial surplus heat is a low-cost and environmentally friendly heat source for DH
 - Use of peak heating sources increases the costs and environmental impact of the heat production significantly
- TES with regular control strategy appears to have a limited possibility to reduce the use of peak heating sources
 - Only 7 % reduction in peak heating
 - In addition: challenging to control the temperature in the tank
- Combining TES with MPC changes the picture:
 - Leveraging demand predictions and optimizing control inputs is key to utilizing TES and minimizing necessary peak heating!
- Future work
 - Calculating the potential cost reduction and payback time for a TES tank
 - Optimal tank dimension for total cost optimality



Thank you for your attention.

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